

Lecture 9 How to calculate

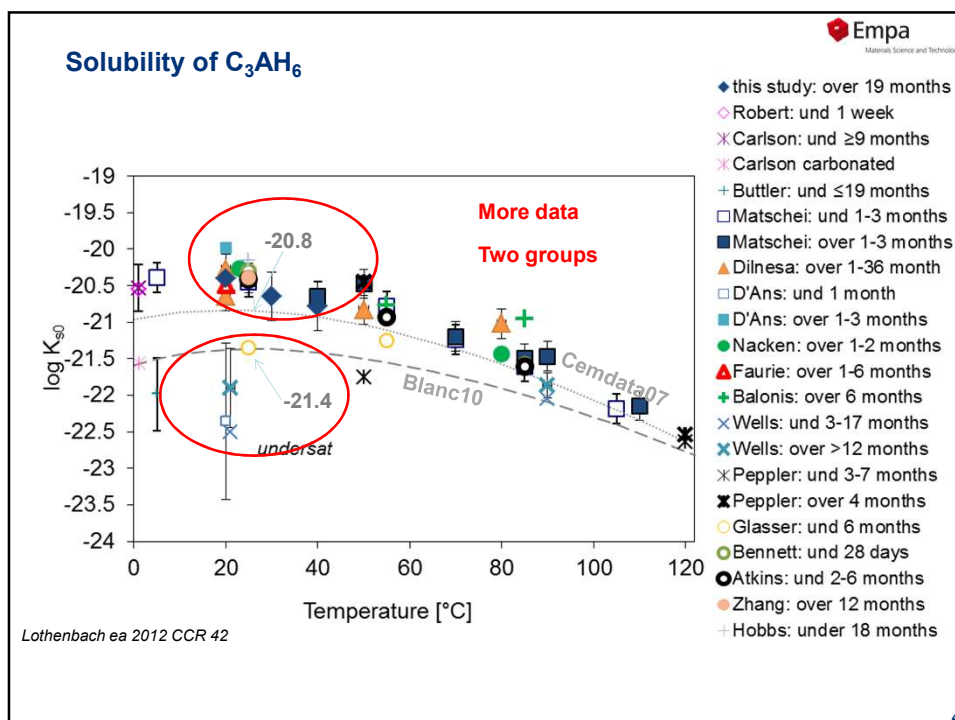
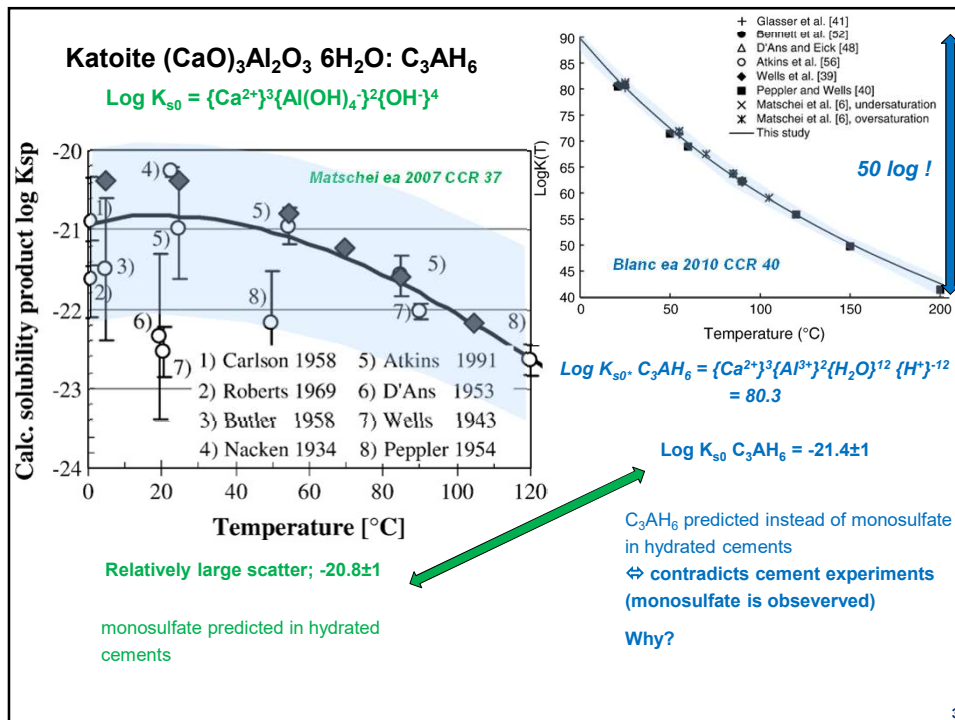


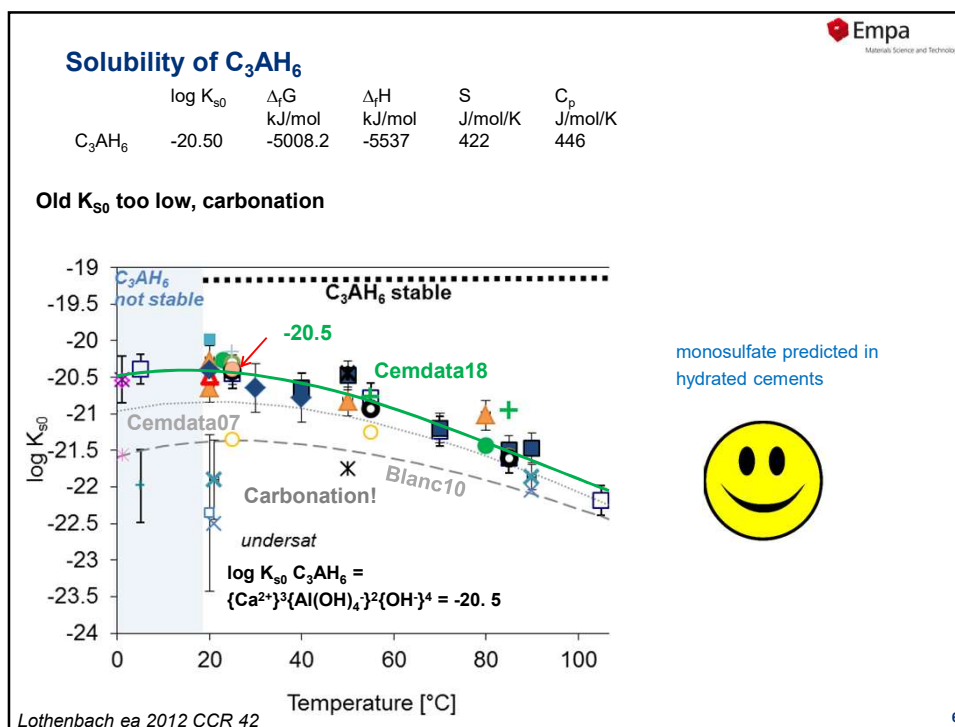
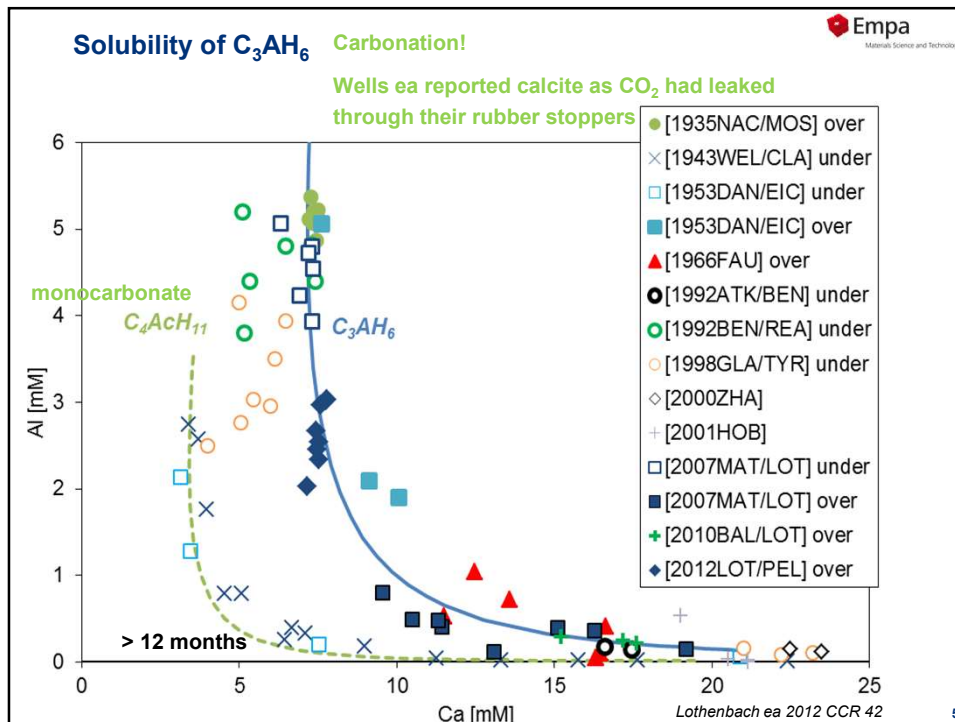
solubility products

Barbara Lothenbach

Solubility products

1. General considerations
2. Measured concentrations
 $\Leftrightarrow \log K_s$
3. Estimation of C_p and S
4. Calculation of $\log K_s$ at different temperatures





Solubility products

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4. Calculation of $\log K_s$ at different temperatures

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Solubility of C_3AH_6

Matschei et al 2007 CCR 37

Table 5

Solubility data for C_3AH_6 at different temperatures and ages

Age [Day]	Temperature [°C]	Ca [mmol/l]	Al [mmol/l]	pH	$\log K_{sp}$	Phases
<i>C_3AH_6 (samples cooled down from initially ~ 105 °C)</i>						
28	25	6.91	4.24	11.91 (11.98 ¹)	-20.52	n.d.
56	25	7.29	4.80	11.92 (11.90 ²)	-20.34	n.d.
84	25	6.31	5.07	11.81 (11.79 ³)	-20.84	C_3AH_6
<i>C_3AH_6 (from undersaturation)</i>						
28	25	7.20	4.73	11.91 (11.96 ¹)	-20.38	n.d.
56	25	7.34	4.55	11.93 (11.90 ²)	-20.32	n.d.
84	25	7.31	3.94	11.95 (11.91 ³)	-20.36	C_3AH_6

undersaturation

Table 3

Experimental data and calculated values of pH and log ion activity product (IAP) for hydrogarnet. Concentrations in mmol dm⁻³

Determination	Ca	Al	OH	pH	log IAP
1	7.43	4.40	23.4	11.66	80.45
2	7.31	4.81	27.0	11.80	81.02
3	5.11	5.20	23.3	11.32	78.89
4	5.16	3.80	23.4	11.83	80.54
5	6.49	4.80	29.6	11.93	81.34
6	5.33	4.40	28.1	11.95	81.12
Average					80.55
Model results	5.75	3.83		11.80	80.55

Bennet et al 1992 J. Nucl Mat 190
redispersion

$$\log K_{s0} = \{Ca^{2+}\}^3 \{Al(OH)_4\}^2 \{OH\}^4$$

$$= -20.8$$

$$\log K_{s0} \cdot C_3AH_6 = \{Ca^{2+}\}^3 \{Al^{3+}\}^2 \{H_2O\}^{12} \{H^+\}^{-12}$$

$$= 80.3$$

$$\text{Differenz} = -(2 \cdot Al(OH)_4^- + 4 \cdot OH^-) = -(2 \cdot -22.9 + 4 \cdot -14) = 101.8$$

Product Substance	Reaction	$\log_{10} K_{298}^\circ$
Al + 3	$AlO_2^- + 4H^+ = Al + 3 + 2H_2O$	22.9
OH-	$H_2O = OH^- + H^+$	-14.0

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Solubility of C₃AH₆

Table 5
Solubility data for C_3AH_6 at different temperatures and ages

Age	Temperature	Ca	Al	pH	Log K_{sp}	Phases
[Day]	[°C]	[mmol/l]	[mmol/l]			
<i>C₃AH₆ (samples cooled down from initially ~ 105 °C)</i>						
28	25	6.91	4.24	11.91 (11.98 ¹)	-20.52	n.d.
56	25	7.29	4.80	11.92 (11.90 ²)	-20.34	n.d.
84	25	6.31	5.07	11.81 (11.79 ³)	-20.84	C ₃ AH ₆
<i>C₃AH₆ (from undersaturation)</i>						
28	25	7.20	4.73	11.91 (11.96 ¹)	-20.38	n.d.
56	25	7.34	4.55	11.93 (11.90 ²)	-20.32	n.d.
84	25	7.31	3.94	11.95 (11.91 ³)	-20.36	C ₃ AH ₆

undersaturation

Table 3
Experimental data and calculated values of pH and log ion activity product (IAP) for hydrogarnet. Concentrations in mmol dm⁻³

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4	5.16	3.80	23.4	11.83	80.54
5	6.49	4.80	29.6	11.93	81.34
6	5.33	4.40	28.1	11.95	81.12
Average					80.55
Model results	5.75	3.83		11.80	80.55

Bennet et al 1992 J. Nucl Mat 190
redispersion

Oversaturation

Table A.7: Solubility data of nominally hydroxy-AFm (C_4AH_{13}) at 25 °C

C ₄ AH ₁₃ (from supersaturation)						
Age [d]	Temp. [°C]	Ca [mmol/l]	Al [mmol/l]	pH	Log K _{sp}	Phases
28	25	17.64	0.21	12.44(12.40)	-25.60	C ₄ AH ₁₃ , C ₃ AH ₆
56	25	20.11	0.20	12.49(12.46)	-25.21	C ₄ AH ₁₃ , C ₃ AH ₆
373	25	19.91	0.17	12.48(12.43)	(-25.38)	C ₃ AH ₆ , Ca(OH) ₂ , C ₄ AH ₁₃ (res)
750	25	19.96	0.09	12.49(12.49)	(-25.93)	C ₃ AH ₆ , Ca(OH) ₂ , C ₄ AH ₁₃ (res)

Thesis Matschei 2008

Solubility of C₃AH₆

 Project: Enter a new record key, please

C3AH6:My1stProject:

C3AH6

Name of the modeling project

Comment to the project definition

Solub

Reset

From List

Step 2: Select Independent Components (not available if shown in light

	I	II	III	IV	V	VI	VII	VIII
1	H							He
2	Li	Be	B	C	N	O	F	Ne
3	Na	Mg	Al	Si	P	S	Cl	Ar
4	K	Ca	Sc	Ti	V	Cr	Mn	Fe
4a	Cu	Zn	Ga	Ge	As	Se	Br	Kr

Setup of aqueous and gas phases in project: C3AH6

Select Aqueous Electrolyte Model | Select Gas/Fluid M

- ☐ Ion-association (IA) with Davies equation, D (default)
- ☒ IA with extended Debye-Hueckel equation (Helgeson), common b_{γ} and a_0 , H
- ☐ IA with extended Debye-Hueckel equation (Shvarov), common b_{γ} and a_0 , Y
- ☐ IA with extended Debye-Hueckel equation (Karpov), common b_{γ} , individual a_0 , 3
- ☐ IA with Debye-Hueckel equation, no b_{γ} , individual a_0 , 2
- ☐ IA with Debye-Hueckel limiting law (very low ionic strength), 1

☐ Do not generate; select a user-defined Phase record from database (0, 5, 7) 1

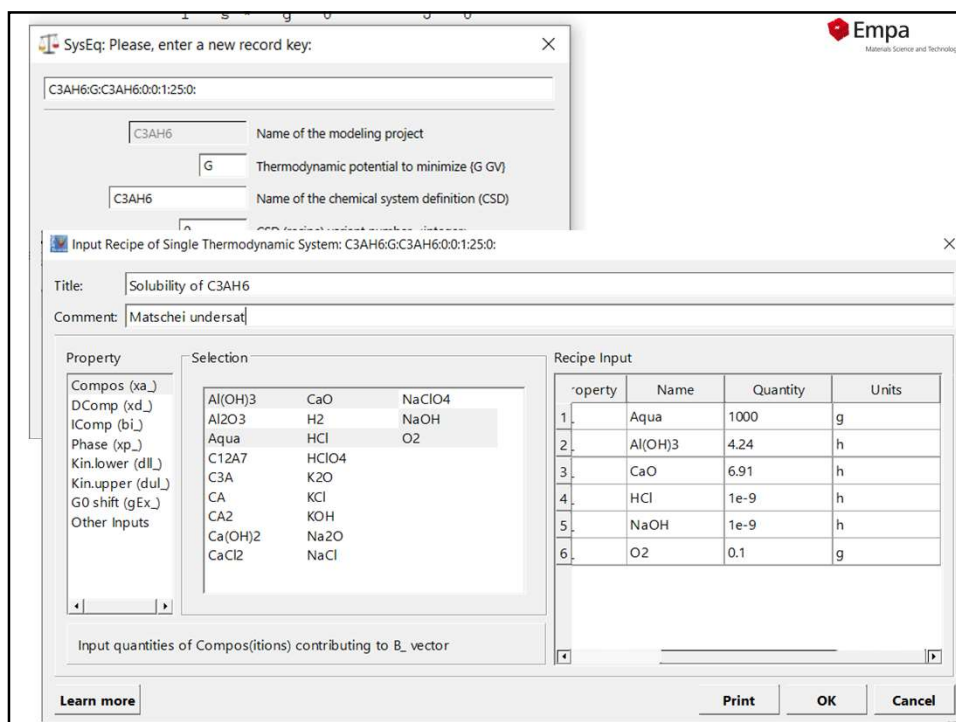
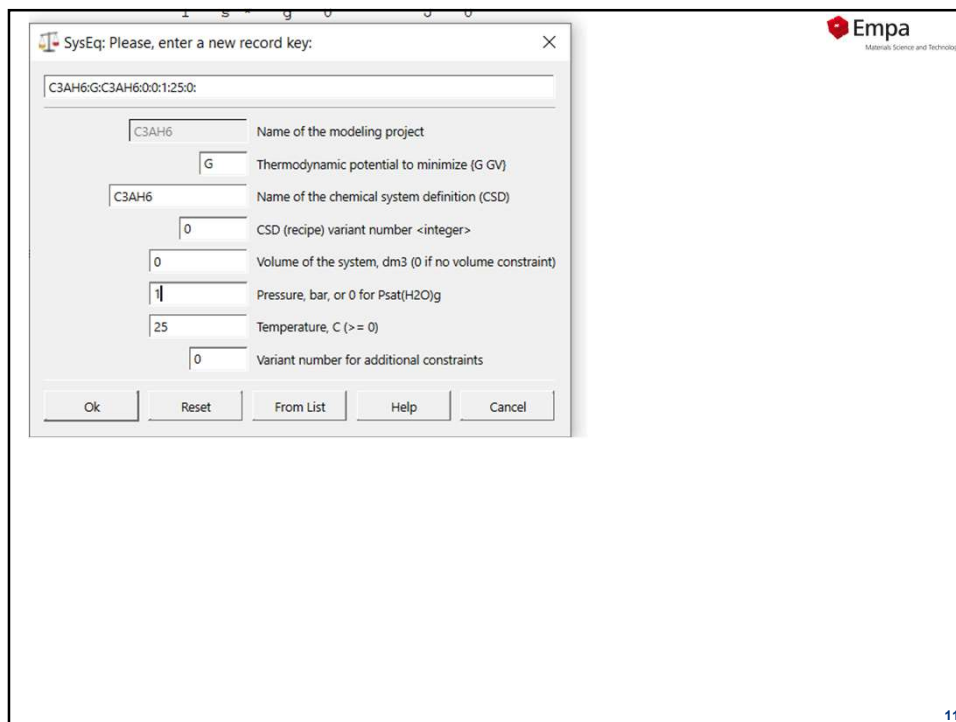
Parameters for
the aqueous phase model

b_gamma(1,298) value:

h. gamma(P,T) mode

Common a0 value:

**NaCl
activity
model**



C3AH6:G:C3AH6:0:0:1:25:0:

Missing ICs **CONFLICT WARNING!**

☐ K

Mole amounts of some Independent Components (IC) are missing in the calculated bulk composition vector ($B_{[i]} < Pa_DB$)!

POSSIBLE ACTIONS:

- * EXCLUDE ALL these ICs together with DCs that contain them and some Phases made of those DCs;
- * RETAIN ALL missing ICs by inserting a default mole amount (below) into bi_vector cells;
- * CHECK some boxes to keep these ICs in the system by inserting a default mole amount into bi_vector ; unchecked ICs will be turned off together with all DCs that contain them.

Default amount, mol (editable):

EXCLUDE ALL **RETAIN ALL** **CHECK/Ok** **Learn more...** **Cancel**

Converged at DK=9.99999e-06

GEM IPM calculation (run time: 0.002 s).

100%

System:

C3AH6:G:C3AH6:0:0:1:25:0:

Iter	1: 13: 96
Gaseous	0.0605419
Aqueous	1000.5
Liquid	0
Solid	0.259173
Total mass	
pH	12.0263
pe	8.74624
IS	0.0192959

Accept **Dismiss**

Compos **DComp 2** **Phase** **IComp** **Surfaces** **Config** 17/05/2023, 09:05

37	-	d	s	KO	K2O	...	M	0	0
38	+	d	s	NaO	Na2O	...	M	0	0

mDCC	DCvp	d11	dul
9 S	a Na Na+	0	1000000 M
10 S	a Na NaOH	0	1000000 M
11 S	a wCl+7 ClO4-	0	1000000 M
12 S	a wCl-1 Cl-	0	1000000 M
13 S	a wH0 H2	0	1000000 M
14 S	a wO0 O2	0	1000000 M
15 S	a wX OH-	0	1000000 M
16 T	a w_ H+	0	1000000 M
17 W	a w_ H2O	0	1000000 M
18 G	g H0 H2	0	1000000 M
19 G	g O0 O2	0	1000000 M
20 G	g Steam H2O	0	1000000 M
21 O	s AlOH AlOHam	0	0 M
22 O	s AlOH AlOHmic	0	0 M
23 O	s AlOH Gbs	0	0 M
24 O	s CaAlO C12A7	0	0 M
25 O	s CaAlO C3A	0	0 M
26 O	s CaAlO CA	0	0 M
27 O	s CaAlO CA2	0	0 M
28 O	s CaAlOH C2AH7.5	0	0 M
29 O	s CaAlOH C3AH6	0	0 M
30 O	s CaAlOH C4AH11	0	0 M
31 O	s CaAlOH C4AH13	0	0 M

dul of all solids = 0
suppresses solid formation

GEM IPM calculation (run time: 0.001 s).

100%

System:

C3AH6:G:C3AH6:0:0:1:25:0:

Iter	1: 15: 29
Gaseous	0.0605576
Aqueous	1000.76
Liquid	0
Solid	0
pH	11.8959
pe	8.8766
IS	0.0196398

Accept
Dismiss

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Matschei et al 2007 CCR 37

Table 5
Solubility data for C_3AH_6 at different temperatures and ages

Age [Day]	Temperature [°C]	Ca [mmol/l]	Al [mmol/l]	pH	Log K_{sp}	Phases
<i>C₃AH₆ (samples cooled down from initially ~ 105 °C)</i>						
28	25	6.91	4.24	11.91 (11.98 ¹)	-20.52	n.d.

Experimental data: pH ±0.1 ☺

15

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C3AH6:G:C3AH6:0:0:1:25:0:

EqC EqPh **EqDC** EqSurf EqGen 17/05/2023, 10:19

Solubility of C3AH6
Matschei undersat

	DCham	X	lga	gamma	my
0	Al+3	2.581514e-27	-27.13749	0.2822567	2.581444e-27
1	AlO+	1.319665e-14	-13.93947	0.8711267	1.31963e-14
2	AlO2-	0.004239987	-2.43256	0.8711267	0.004239872
3	AlO2H0	1.309191e-08	-7.88182	1.002908	1.309155e-08
4	AlOH+2	1.108382e-20	-20.19863	0.5708768	1.108352e-20
5	Ca+2	0.006365175	-2.439663	0.5708768	0.006365002
6	CaOH+	0.0005448249	-3.323626	0.8711267	0.0005448101
7	Na+	9.955028e-13	-12.06189	0.8711267	9.954757e-13
8	NaOH0	4.497228e-15	-14.34581	1.002908	4.497106e-15
9	ClO4-	2.921578e-34	-33.59431	0.8711267	2.921495e-34
10	Cl-	1e-12	-12.05993	0.8711267	9.999728e-13
11	H2O	0	-44.65106	1.002908	0
12	O20	0.001267678	-2.895609	1.002908	0.001267644
13	OH-	0.009035188	-2.103996	0.8711267	0.009034943
14	H+	1.458976e-12	-11.89595	0.8711267	1.458937e-12
15	H2O0	55.50988	-0.000154809	1.00003	55.50937

$K_{s0} = \{Ca^{2+}\}^3 \{Al(OH)_4\}^2 \{OH\}^4$
 Convention from SUPCRT used in GEMS
 $Al(OH)_4^{-2} = AlO_2^{-} + 2H_2O^0$

$K_{s0} = \{Ca^{2+}\}^3 \{AlO_2\}^2 \{H_2O^0\}^4 \{OH\}^4$
 $\log K_{s0} = 3 \cdot \lg a Ca^{2+} + 2 \cdot \lg a AlO_2^{-} + 4 \cdot \lg a H_2O^0 + 4 \cdot \lg a OH^{-}$
 $= 3 \cdot -2.44 + 2 \cdot -2.43 + 4 \cdot -0.0002 + 4 \cdot -2.10 = -20.58$

Experimental data: pH 11.98 ☺

1

2

16

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1

2

EqC EqPh **EqDC** EqSurf EqGen 17/05/2023, 10:49

Solubility of C3AH6
Matschei undersat

	DCnam	x	lga	gamma	my
0	Al+3	1.282742e-27	-27.46212	0.2690042	1.282707e-27
1	AlO+	9.106181e-15	-14.10289	0.86669	9.105934e-15
2	AlO2-	0.004239989	-2.434783	0.86669	0.004239874
3	AlO2H8	1.08176e-08	-7.964654	1.003175	1.08173e-08
4	AlOH+2	6.458857e-21	-20.44267	0.5588877	6.458681e-21
5	Ca+2	0.006273697	-2.455159	0.5588877	0.006273527
6	CaOH+	0.000636303	-3.258534	0.86669	0.0006362857
7	Na+	0.001989237	-2.763461	0.86669	0.001989183
8	NaOH8	1.07627e-05	-4.966791	1.003175	1.076241e-05
9	ClO4-	2.922946e-34	-33.59633	0.86669	2.922867e-34
10	Cl-	1e-12	-12.06215	0.86669	9.999728e-13
11	H28	0	-44.65114	1.003175	0
12	O28	0.001268174	-2.895508	1.003175	0.00126814
13	OH-	0.01093295	-2.023408	0.86669	0.01093265
14	H+	1.217925e-12	-11.97656	0.86669	1.217892e-12
15	H2O8	55.50988	-0.0001836641	1.000034	55.50837

pH corrected
+ 2 mmol/L NaOH

$K_{s0} = \{Ca^{2+}\}^3 \{Al(OH)_4\}^2 \{OH\}^4$
Convention from SUPCRT used in GEMS
 $Al(OH)_4^- = AlO_2^- + 2H_2O^0$
 $K_{s0} = \{Ca^{2+}\}^3 \{AlO_2\}^2 \{H_2O^0\}^4 \{OH\}^4$
 $\log K_{s0} = 3 \cdot lga Ca^{2+} + 2 \cdot lga AlO_2^- + 4 \cdot lga H_2O^0 + 4 \cdot lga OH^-$
 $= 3 \cdot -2.46 + 2 \cdot -2.43 + 4 \cdot -0.0002 + 4 \cdot -2.02 = -20.62$: little difference, error ± 1

Experimental data: pH 11.98 ☺

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GEM-Selektor 3 (GEMS3) - Geochemical Equilibrium Modelling by Gibbs Energy Minimization - [Process : Definition of a Process Simulator (batch calculation)]

Modules Record Window Help

Process

3 4 5 6 7 8 9 10

SysEq

Process

GtDemo

Controls Sampling Results Config 17/05/2023, 09:57

SysEq: Please, select a parent System for a new Process

Please, select one record key. Filter: C3AH6:*****:

C3AH6 G C3AH6 0 0 1 25 0

Create a new process file

Process: Please, set a new record key

C3AH6:G:C3AH6:0:1:25:0:Solub:SS:

4

C3AH6 Name of the modeling project

G Thermodynamic potential to minimize (G)

C3AH6 Name of the parent chemical system definition (CSD)

0 CSD (recipe) variant number <integer>

0 Volume of the system, dm3

1 Pressure, bar, or 0 for Psat(H2O)g

25 Temperature, C

0 Variant number for additional constraints

Solub Name of this process simulation task

S Process simulation mode code { P, S, L, G, T, R }

Ok Reset From List Help Cancel

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GEM-Selektor Process Setup: C3AH6G/C3AH6O0:125:0:SolubS:

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Step 2 - Process Simulation Controls (click 'Next' to retain the old script)

	iTm	iV	iP	ITC	iNv	iTau	ipX	iNu	ipH	ipe
From	1000	0	1	25	0	0	0	0	0	0
Until	1200	0	1	25	0	0	0	0	0	0
Step	10	0	0	0	0	0	0	0	0	0

☒ Titration cNu (linear)
 ☐ Diagram logD vs x (linear)
 ☐ Titration cpXi logarithmic
 ☐ Diagram logKd vs log(m)

Linear titration and logD diagrams use the iNu iterator; logarithmic titration and logKd diagrams use ipXi. Titrations: select required titrants as items from 'Compos', 'DComp', 'iComp' or 'Phase' lists, optionally also select items from 'DC-lower' or 'DC-upper' to change metastability constraints.

To plot logD vs linear x (mole fraction) scale: (i) select minor then host end member from the 'DComp' list, (ii) select trace then host ion from the 'Molality' list. To plot logKd and isotherms vs log(molality) scale: (i) select trace then host compositions from the 'Compos' list; (ii) select trace then host elements from the 'Sorbed' list. In both cases, skip the next wizard page.

Compos: Al(OH)3, CaO, NaClO4
 DComp: Al2O3, H2, NaOH
 iComp: Aqua, HCl, O2
 Phases: C12A7, HClO4
 DC-lower: C3A, K2O
 DC-upper: CA, KCl
 Molality: CA2, KOH
 Sorbed: Ca(OH)2, Na2O, CaCl2, NaCl

```
modC[] =: cNu;
xa_[Al(OH)3] =: cNu * 1;
xa_[CaO] =: cNu * 1;
xa_[NaOH] =: cNu * 1;
xa_[HCl] =: cNu * 1;
```

Learn more

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Next>

Cancel

Select Al(OH)3 and CaO as input for measured total Al and Ca (in mM)

NaOH and HCl in case you need to correct the pH

Experimental data: pH ±0.1 ☺

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GEM-Selektor Process Setup: C3AH6G/C3AH6O0:125:0:SolubS:

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Step 3 - Selection of items to sample/plot (click 'Next' without selecting anything to retain the old script)

Property

Scalars

u

ue

b

Cb

m_t

lgm_t

icm

Xa

Xwa

phVol

phM

Pa

bXa(aq_gen)

bXa(gas_gen)

bXs

L1

Yof

Aalp

Sigw

x

Wxx

Item Selection

Mbx	_nnr[0]	F_RT	FL[3]	ITC[
pmXs	_nnr[1]	Xw	T	ITC[1
OX	L[0]	Masses[0]	P	ITC[2
IS	L[1]	Masses[1]	RT[0]	cTC
pH	L[2]	Masses[2]	RT[1]	cT
pe	L[3]	Masses[3]	RowW[0][0]	iNv[1
Eh	L[4]	Masses[4]	EpsW[0][0]	iNv[2
TC[0]	L[5]	Masses[5]	VisW[0]	iNv[3
TC[1]	Fi[0]	Volumes[0]	ITm[0]	cNV
TK[0]	Fi[1]	Volumes[1]	ITm[1]	ITau[
TK[1]	Fi[2]	NL	ITm[2]	ITau[
PG[0]	Fi[0]	L[0]	cTm	ITau[
PG[1]	Fi[1]	L[1]	iV[0]	cTau
Vx[0]	Fi[2]	L[2]	iV[1]	ipX[
Vx[1]	denW[0][0]	L[3]	iV[2]	ipX[
It	denW[1][0]	L[4]	cV	ipX[
ItEfd	epsW[0][0]	L[5]	iP[0]	cpX[
Itipm	epsW[1][0]	FL[0]	iP[1]	cXi
PsL_DK[0]	InP	FL[1]	iP[2]	iNu[
PsL_DK[1]	RT	FL[2]	cP	iNu[

List of static data objects (see tooltip on each object name)

Sampling Script

```
yp[] =: ;
yp[0] =: lga[AlO2-];
yp[1] =: lga[Ca+2];
yp[2] =: lga[OH-];
yp[3] =: lga[H2O@];
yp[4] =: pH;
```

Learn more

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Next>

Cancel

Collect lga[AlO2-], lga[Ca+2], lga[OH-], lga[H2O@] and pH needed to formulate equation

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Step 4 - Important data object dimensions

Spin boxes below define the dynamic memory configuration of the process simulator.

Dimensions of sampled and experimental data

10 nPS - Number of steps (1 to 9999) to be performed in this simulation (default: 21); also length of the 'xp' vector.

4 Number of 'modC' array columns (1 to 40, 0 - not used) to store process control values; number of rows will be nPS.

5 Number of columns in the 'yp' table (0 to 200) to keep the simulated data sampled by the pgExpr script; number of rows will be nPS.

1 Number of columns in the 'xp' table (0 to 4) to keep the simulated data sampled by the pgExpr script; number of rows will be nPS.

10 Number of rows in the xEp, yEp arrays for experimental data (optional)

1 Number of columns in the xEp, yEp arrays for experimental data (optional)

Optional data vectors (of length nPS) can be used for accumulating current process control values for all steps performed. They can be allocated using checkboxes below. The assignment operator (with J index) in the script will override any values automatically copied into data vector from the respective process iterator.

Allocation of optional data vectors

☐ CSD variant # (vTm)

☐ Volume V, l (vV)

☐ Pressure P, bar (vP)

☐ Temperature T (vT)

☐ Constraints # (vNV)

☐ Process extent Nu (vNu)

☐ Process extent pXi (vpXi)

☐ Kinetic parameters (vKin)

☐ Time Tau (vTau)

Learn more
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Next->
Cancel

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10 experimental data points from Matschei

4 columns for input: Al, Ca, NaOH and HCl

5 output columns

1 X-axis

10 experimental pH values for comparison

1 experimental column for pH values

21

Controls Sampling Results Config 17/05/2023, 09:57

Solubility C3AH6

Data Matschei (6 from undersat, 4 from oversaturation)

	iTm	iV	iP	iTC	iNV	iTau	ipXi	iNu	ipH	ipe
0	1000	0	1	25	0	0	0	0.1	0	0
1	1031	0	1	25	0	0	0	3.1	0	0
2	1	0	0	0	0	0	0	0.1	0	0
cTm	1000	0	1	25	0	0	0	0.1	0	0

```

SmodC[J] =: cNu;
$ input of totalconc in mM
xa_[(Al(OH)3)] =: modC[J][0];
xa_[(CaO)] =: modC[J][1];
$ often not needed, for pH correction
xa_[(NaOH)] =: modC[J][2];
xa_[(HCl)] =: modC[J][3];

```

	modC[0]	modC[1]	modC[2]	modC[3]
0	4.24	6.91	1e-09	1e-05
1	4.8	7.29	1e-09	1e-05
2	5.07	6.31	1e-09	1e-05
3	4.73	7.2	1e-09	1e-05
4	4.55	7.34	1e-09	1e-05
5	3.94	7.31	1e-09	1e-05
6	0.21	17.64	1e-09	1e-05
7	0.2	20.11	1e-09	1e-05
8	0.17	19.91	1e-09	1e-05
9	0.09	19.96	1e-09	1e-05

Input in mM

modC[J][0] = total Al measured

modC[J][1] = total Ca measured in mM

modC[J][2], and modC[J][3] = 10⁻⁹ mM (use small numbers not «0»)

22

Controls		Sampling		Results		Config		17/05/2023, 11:21		
NeIt	9999	0	Next	1	I	0	J	0	Jp	0
pStkey	C3AH6:G:C3AH6:0:0:1:25:0:						cTm	1000	cNV	
cTau	0	cpXi	0	cXi	1	cNu				
cpH	0	cpe	0	cEh	0	cT				


```

xp[J] =: J;
$ J: calculation number
yp[J][0] =: 3*log[Ca+2]+2*log[AlO2-]+4*log[OH-]+4*log[H2O@];
yp[J][1] =: 0;
yp[J][2] =: 0;
yp[J][3] =: 0;
yp[J][4] =: pH;

xp[J] =: J; $ J: calculation number

Calculation of solubility product of C3AH6
yp[J][0] =: 3*log[Ca+2]+2*log[AlO2-]+4*log[OH-]+4*log[H2O@];
yp[J][1] =: 0;
yp[J][2] =: 0;
yp[J][3] =: 0;
yp[J][4] =: pH; => used for comparison with measured pH

Label to first column as K C3AH6

```

Emna

ling	Results	Config	17/05/2023, 11:21																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
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Error on solubility products (assuming normal distribution)

see also https://www.oecd-nea.org/jcms/pl_37493/tdb-3-guidelines-for-the-assignment-of-uncertainties

Measurement error

Standarddeviation: in excel use **STDEV.S**

$$s_X = \sqrt{\frac{1}{N-1} \sum_{i=1}^N (X_i - \bar{X})^2}$$

Uncertainty (includes also systematic errors, s_i)

$$\sigma_{\bar{X}} = \sqrt{s_X^2 + \sum_j (s_j^2)}$$

95% confidence interval

$$95\% \text{ Confidence Interval} = \bar{x} \pm t(\sigma / \sqrt{n})$$

T value for n-1 from table

[illegible]

Do and do not

- Do not use the mean of all measurements to calculate one solubility product

	Al	Ca		
Undersat	4.24	6.91		
	4.8	7.29		
	5.07	6.31		
	4.73	7.2		
	4.55	7.34		
	3.94	7.31		
Oversat	0.21	17.64		
	0.2	20.11		
	0.17	19.91		
	0.09	19.96		
mean				
undersat	4.56	7.06	-20.52	1.5
oversat	0.17	19.41	-20.40	3.5
all	2.8	12.00	-19.25	14.2
standard dev	2.3	6.4		

- Use the log of the individual solubility products to calculate the mean

	-20.60
	-20.42
	-20.92
	-20.46
	-20.40
	-20.44
	-20.43
	-20.18
	-20.34
	-20.89
Mean	-20.51
Standard deviation	0.23
confidence interval (95%, 2 sided)	0.17



GEM-Selektor 3 (GEMS3) - Geochemical Equilibrium Modelling by Gibbs Energy Minimization - [Process - Definition of a Process Simulator (batch calculation)]

Modules Record Window Help

Process C3AH6:*****

Controls Sampling Results Config 17/05/2023, 09:57

SysEq: Please, select a parent System for a new Process

Please, select one record key. Filter: C3AH6:*****:

C3AH6	G	C3AH6	0	0	1	25	0
Create a new process file							

Process: Please, set a new record key

C3AH6:G:C3AH6:0:0:1:25:0:Solub 2:S

4

C3AH6 Name of the modeling project

G Thermodynamic potential to minimize {G}

C3AH6 Name of the parent chemical system definition (CSD)

0 CSD (recipe) variant number <integer>

0 Volume of the system, dm3

1 Pressure, bar, or 0 for Psat(H2O)g

25 Temperature, C

0 Variant number for additional constraints

Solub 2 Name of this process simulation task

S Process simulation mode code { P, S, L, G, T, R }

Ok Reset From List Help Cancel

Do not change anything,

27

Step 4 - Important data object dimensions

Spin boxes below define the dynamic memory configuration of the process simulator.

Dimensions of sampled and experimental data

7 nPS - Number of steps (1 to 9999) to be performed in this simulation (default: 21); also length of the 'xp' vector

4 Number of 'modC' array columns (1 to 40, 0 - not used) to store process control values; number of rows will be nPS.

5 Number of columns in the 'yp' table (0 to 200) to keep the simulated data sampled by the pgExpr script; number nPS.

1 Number of columns in the 'xp' table (0 to 4) to keep the simulated data sampled by the pgExpr script; number nPS.

7 Number of rows in the xEp, yEp arrays for experimental data (optional)

1 Number of columns in the xEp, yEp arrays for experimental data (optional)

Optional data vectors. (of length nPS) can be used for accumulating current process control values for all steps performed. 1 allocated using checkboxes below. The assignment operator (with j index) in the script will override any values automatically, vector from the respective process iterator.

Allocation of optional data vectors

☐ CSD variant # (vVm) ☐ Volume V, l (vV) ☐ Pressure P, bar (vP)

☐ Temperature T (vT) ☐ Constraints # (vNV) ☐ Process extent Nu (vNu)

☐ Process extent pXi (vXi) ☐ Kinetic parameters (vKin) ☐ Time Tau (vTau)

Learn more < Back Next> Cancel


Table 3
Experimental data and calculated values of pH and log ion activity product (IAP) for hydrogarnet. Concentrations in mmol dm⁻³

Determination	Ca	Al	OH	pH	log IAP
1	7.43	4.40	23.4	11.66	80.45
2	7.31	4.81	27.0	11.80	81.02
3	5.11	5.20	23.3	11.32	78.89
4	5.16	3.80	23.4	11.83	80.54
5	6.49	4.80	29.6	11.93	81.34
6	5.33	4.40	28.1	11.95	81.12
Average					80.55
Model results	5.75	3.83		11.80	80.55

Bennet ea 1992 J. Nucl Mat 190 redispersion

6+1 experimental data points from Bennet
4 columns for input: Al, Ca, NaOH and HCl
5 output columns
1 X-axis
6+1 experimental pH values for comparison
1 experimental column for pH values

28



 Materials Science and Technology

Solubility C3AH6
 Data Bennet (6 from undersat redispersion, 1 mean)

	iTm	iV	iP	iTC	iNv	iTau	ipXi	iNu	ipH	ipe
0	1000	0	1	25	0	0	0	0.1	0	0
1	1031	0	1	25	0	0	0	3.1	0	0
2	1	0	0	0	0	0	0	0.1	0	0
cTm	1000	0	1	25	0	0	0	0.1	0	0

```

$modC[J] =: cNu;
$ input of totalconc in mM
xa_{{Al(OH)3}} =: modC[J][0];
xa_{{CaO}} =: modC[J][1];
$ often not needed, for pH correction
xa_{{NaOH}} =: modC[J][2];
xa_{{HCl}} =: modC[J][3];

$ last is mean, for comparison only
          
```

	modC[0]	modC[1]	
0	4.4	7.43	
1	4.81	7.31	
2	5.2	5.11	
3	3.8	5.16	
4	4.8	6.49	
5	4.4	5.33	
6	3.83	5.75	


Input in mM

modC[J][0] = total Al measured

modC[J][1] = total Ca measured in mM

modC[J][2], and modC[J][3] = 10⁻⁹ mM (use small numbers not «0»)

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 Materials Science and Technology

Solubility C3AH6

Sampling | Results | Config | 17/05/2023, 17:44

solubility C3AH6
pY_Nam ordinate

am	abscissa	K C3AH6	Ca+2	OH-	H2O@	pH		abscissa	pH
0	0	-20.36573	0	0	0	11.93112	0	0	11.66
1	1	-20.40765	0	0	0	11.90379	1	0	11.8
2	2	-21.75947	0	0	0	11.62643	2	0	11.32
3	3	-21.57668	0	0	0	11.74005	3	0	11.83
4	4	-20.80627	0	0	0	11.82964	4	0	11.93
5	5	-21.49081	0	0	0	11.72102	5	0	11.95
6	6	-21.20783	0	0	0	11.80663	6	0	11.8

K C3AH6 = solubility product of C3AH6

yp[J][0] =: 3*Iga[{{Ca+2}}]+2*Iga[{{AlO2-}}]+4*Iga[{{OH-}}]+4*Iga[{{H2O@}}];

Varies from -20.3 to -21.8

Decreases with time. Carbonation!

Calculated pH ≈ comparable to measured pH

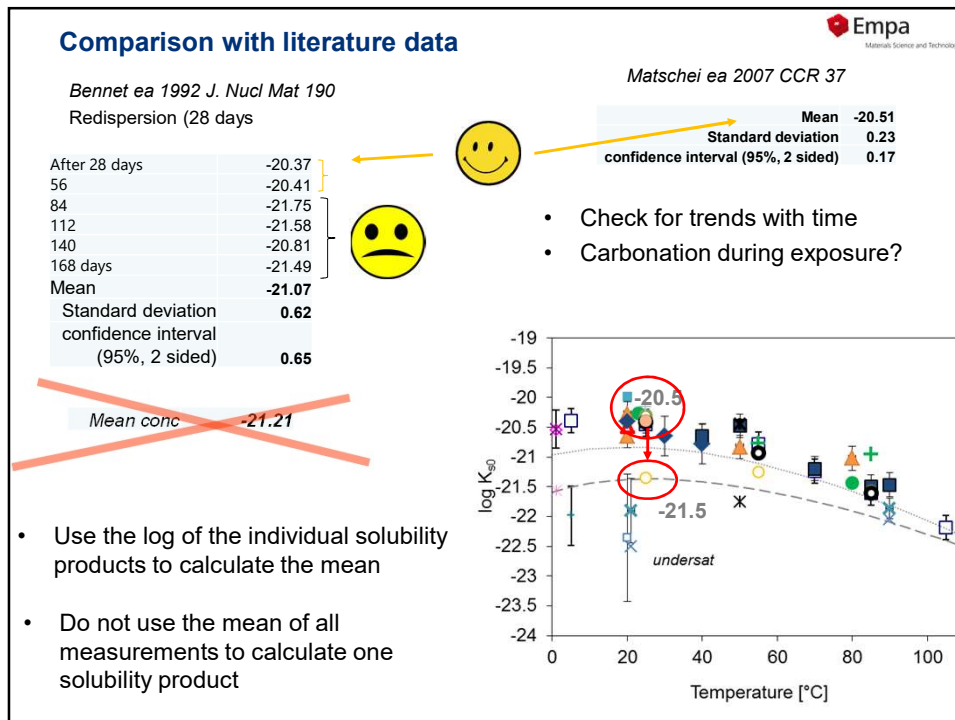
Δ pH ± 0.3 => No pH correction done

(pH difficult to measure, least reliable, avoid if difference not too large)

With pH correction -20.6 to -23.0)

solubility C3AH6
pY_Nam ordinate

am	abscissa	K C3AH6	Ca+2	OH-	H2O@	pH		abscissa	pH
0	0	-21.45787	0	0	0	11.64714	0	0	
1	1	-20.78876	0	0	0	11.80412	1	0	
2	2	-22.99794	0	0	0	11.30874	2	0	
3	3	-21.36384	0	0	0	11.80088	3	0	
4	4	-20.55935	0	0	0	11.90139	4	0	
5	5	-20.76407	0	0	0	11.93134	5	0	



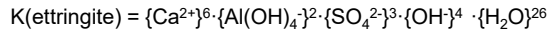
Empa
Materials Science and Technology

Solubility products

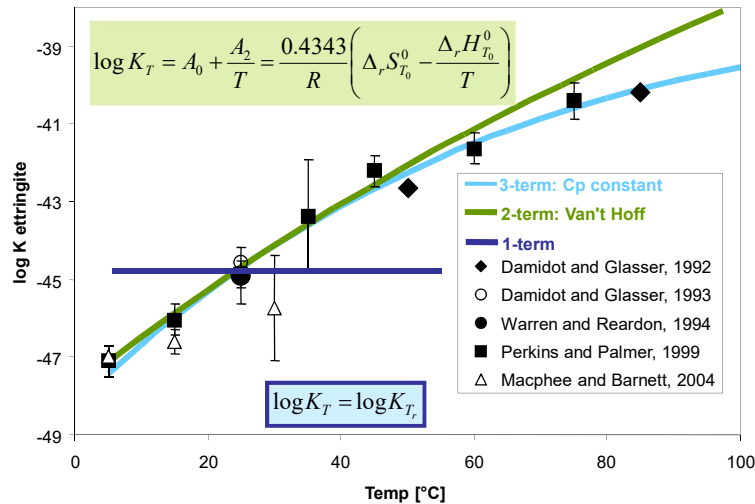
1. General considerations
2. Measured concentrations
 $\Leftrightarrow \log K_s$
3. Estimation of C_p and S
4. Calculation of $\log K_s$ at different temperatures

32

Effect of temperature



$$\log K_T = A_0 + A_2 T^{-1} + A_3 \ln T$$



Lothenbach et al. CCR 38, 2008

33

Thermodynamic data:

$$K_T = e^{-\frac{\Delta_r G_T^{\circ}}{RT}}$$

$K_{S0} \leftrightarrow$ Gibbs free energy

$$\Delta_r G_T^{\circ} = \sum_i \nu_i \Delta_f G_T^{\circ}$$

Influence of temperature $\log K_T = A_0 + \frac{A_2}{T} + A_3 \ln T$

$$A_0 = \frac{0.4343}{R} \cdot \left[\Delta_r S_{T_0}^0 - \Delta_r C p_{T_0} (\ln T_0 + 1) \right]$$

$$A_2 = -\frac{0.4343}{R} \cdot (\Delta_r H_{T_0}^0 - \Delta_r C p_{T_0} T_0)$$

$$A_3 = \frac{0.4343}{R} \cdot \Delta_r C p_{T_0} = \frac{0.4343}{8.3145} \cdot -391.1 = -20.43$$

34

We can estimate S and Cp (but better not ΔH_f and ΔG_f)

1) From similar solids (avoiding liquid water)

H.C. Helgeson, J.M. Delany, H.W. Nesbitt, D.K. Bird, *Summary and critique of the thermodynamic properties of rock-forming minerals*, Am J Sci, 278-A (1978) 1-229

G.M. Anderson, D.A. Crerar, *Thermodynamics in Geochemistry: the Equilibrium Model*, Oxford University Press, Oxford, 1993.

2) Volume based thermodynamics (VBT)

L. Glasser, *The effective volumes of waters of crystallization & the thermodynamics of cementitious materials*, Cement, 3 (2021) 100004.

S. Ghazizadeh, T. Hanein, J.L. Provis, T. Matschei, *Estimation of standard molar entropy of cement hydrates and clinker minerals*, Cem Concr Res, 136 (2020) 106188.

L. Glasser, H.D.B. Jenkins, *Predictive thermodynamics for ionic solids and liquids*, Physical Chemistry Chemical Physics, 18 (2016) 21226-21240.

35

We can estimate S and Cp (but better not ΔH_f and ΔG_f)

1) From similar solids (avoiding liquid water)

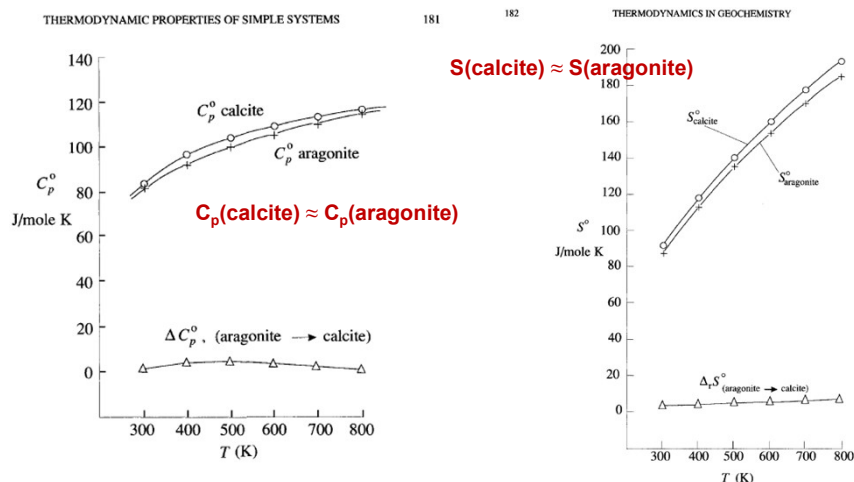


FIG. 7.10. Heat capacities of calcite and aragonite, showing that ΔC_p° varies much less than either C_p° .

FIG. 7.11. Entropies of calcite and aragonite, showing that ΔS° varies much less than either S° .

G.M. Anderson, D.A. Crerar, *Thermodynamics in Geochemistry: the Equilibrium Model*, Oxford University Press, Oxford, 1993

36

We can estimate Cp

1) From similar solids (avoiding liquid water)

$$C_{p,T_r,i}^{\circ} = \sum_j \nu_{j,i} C_{p,T_r,j}^{\circ} \quad (78)$$

H.C. Helgeson, J.M. Delany, H.W. Nesbitt,
D.K. Bird, *Am J Sci*, 278-A (1978) 1-229

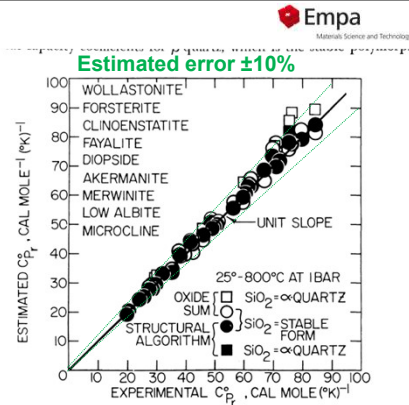


Fig. 11. Correlation of estimated and experimental standard molar heat capacities of minerals at 25°, 200°, 500°, and 800°C at 1 bar.

$$C_{p,C3AH} \approx 3 \cdot C_{p,CH} + 2 \cdot C_{p,Al(OH)_3} = 3 \cdot 87.51 + 2 \cdot 93.08 = 449 \pm 45 \text{ J/mol/K}$$

$$C_{p,C3AH6} \approx C_{p,C3A} + 6 \cdot C_{p,\text{structural H}_2O} = 209.39 + 6 \cdot 40.04 = 450 \pm 45 \text{ J/mol/K}$$

$$C_{p,C3AH6, \text{measured}} \approx 446 \text{ (Geiger 2012), or } 459 \text{ (Ederova 1979) J/mol/K}$$

Good agreement (estimation, measured values preferred)

J. Ederova, V. Satava, *Heat capacities of C_3AH_6 , C_4ASH_{12} and $C_6AS_3H_{32}$* , *Thermochim Acta*, 31 (1979) 126-128.

C.A. Geiger, E. Dachs, A. Benisek, *Thermodynamic behavior and properties of katoite (hydrogrossular): A calorimetric study*, *Am Min*, 97 (2012) 1252-1255.

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Summary of experimental standard molal volumes, entropies, and heat capacity power function coefficients for oxides

Mineral	Formula	V_{P,T_r}^a	S_{P,T_r}^b	$C_{P,T_r}^{b \cdot D}$	Coefficients for equation (19)			Temperature Range, °K
					$\frac{a}{b}$	$\frac{b \cdot 10^3}{c \cdot 10^{10}}$	$\frac{c \cdot 10^{-5}}{d \cdot 10^{-10}}$	
"Structural" H ₂ O	H ₂ O _(s)	13.7 ^m	9.6 ⁿ	9.57	7.11 ^z	8.24 ^z	0.00 ^z	298-1000 ^z
"Zeolitic" H ₂ O	H ₂ O _(z)	8 ^z	14.1 ^z	11.4	11.4 ^z	0.0 ^z	0.0 ^z	

$a = \text{cm}^3 \text{ mole}^{-1}$, $b = \text{cal mole}^{-1} (\text{°K})^{-1}$, $c = \text{Estimated from standard molal volumes of zeolites (see text)}$,
 $d = \text{cal mole}^{-1} (\text{°K})^{-2}$, $e = \text{cal} (\text{°K}) \text{ mole}^{-1}$, ^mRobie and Waldbaum (1968), ⁿStull and

H.C. Helgeson, J.M. Delany, H.W. Nesbitt, D.K. Bird, *Am J Sci*, 278-A (1978) 1-229

cal/mol/K

*4.184 => J/mol/K

Where do we get the data from ?

J/mol/K

B. Lothenbach, D. Kulik, T. Matschei, M. Balonis, L.G. Baquerizo, B.Z. Dinesa, G.D. Miron, D. Myers, *Cemdata18: A chemical thermodynamic database for hydrated Portland cements and alkali-activated materials*, *Cem Concr Res*, 115 (2019) 472-506

We can estimate S

1) From similar solids (avoiding liquid water)

$$S_{i,P_r,T_r}^{\circ} = \frac{S_{s,i,P_r,T_r}^{\circ} (V_{s,i,P_r,T_r}^{\circ} + V_{i,P_r,T_r}^{\circ})}{2V_{s,i,P_r,T_r}^{\circ}} \quad (62)$$

H.C. Helgeson, J.M. Delany, H.W. Nesbitt,
D.K. Bird, *Am J Sci*, 278-A (1978) 1-229

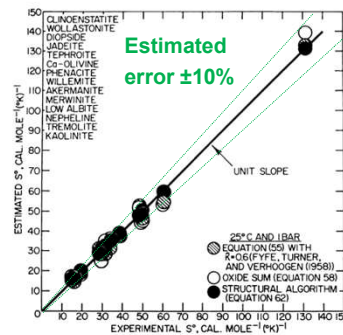


Fig. 10. Correlation of estimated and experimental standard molal entropies of minerals at 25°C and 1 bar.

$$S_{C3AH6} \approx (3 \cdot S_{CH} + 2 \cdot S_{AH1.5}) \cdot (3 \cdot V_{CH} + 2 \cdot V_{AH1.5} + V_{C3AH6}) / 2 / (3 \cdot V_{CH} + 2 \cdot V_{AH1.5}) =$$

$$(3 \cdot 83.4 + 2 \cdot 70.08) \cdot (3 \cdot 33.1 + 2 \cdot 32.0 + 149.7) / 2 / (3 \cdot 33.1 + 2 \cdot 32.0) = 390.4 \cdot 0.96 = 374 \pm 37 \text{ J/mol/K}$$

$$S_{C3AH6} \approx (S_{C3A} + 6 \cdot S_{stH2O}) \cdot (V_{C3A} + 6 \cdot V_{stH2O} + V_{C3AH6}) / 2 / (V_{C3A} + 6 \cdot V_{H2O}) =$$

$$(205.4 + 6 \cdot 40.2) \cdot (89.2 + 6 \cdot 13.8 + 149.7) / 2 / (89.2 + 6 \cdot 13.8) = 446.4 \cdot 0.94 = 418 \pm 42 \text{ J/mol/K}$$

$$S_{C3AH6, \text{measured}} \approx 422 \text{ (Geiger 2012) J/mol/K}$$

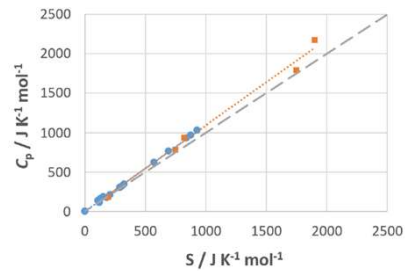
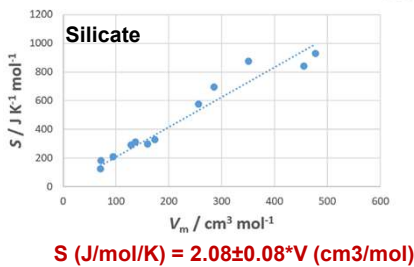
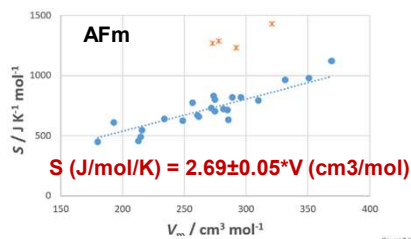
Adequate agreement (estimation, measured values preferred)

C.A. Geiger, E. Dachs, A. Benisek, *Thermodynamic behavior and properties of katoite (hydrogrossular): A calorimetric study*, *Am Min*, 97 (2012) 1252-1255.

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We can estimate S and Cp (but better not ΔH_f and ΔG_f)

2) Volume based thermodynamics (VBT)



$$C_p \text{ (J/mol/K)} = 1.1 \cdot S \text{ (J/mol/K)}$$

L. Glasser, *The effective volumes of waters of crystallization & the thermodynamics of cementitious materials*, *Cement*, 3 (2021) 100004.

40

We can estimate S

2) Volume based thermodynamics (VBT); $V_{C_3AH_6} = 149 \text{ cm}^3/\text{mol}$	J/mol/K
S (J/mol/K) = $2.69 \pm 0.05 \cdot V \text{ (cm}^3/\text{mol)}$ for AFm, Glasser 2021)	403 ± 7
<i>S (J/mol/K) = $2.08 \pm 0.08 \cdot V \text{ (cm}^3/\text{mol)}$ for crystalline CSH, Glasser 2021)</i>	<i>311 ± 12</i>
<i>S (J/mol/K) = $2.26 \pm 0.09 \cdot V \text{ (cm}^3/\text{mol}) + 15 \pm 6 \text{ anhydrous solid, Glasser 2016)}$</i>	<i>353 ± 42</i>
S (J/mol/K) = $2.62 \pm 0.05 \cdot V \text{ (cm}^3/\text{mol}) + 6 \pm 6 \text{ hydrous solid,}$ (Glasser ea 2016, Gahzizadeh ea 2020)	399 ± 29
S (J/mol/K) = from similar solids	374 ± 37 418 ± 42

$S_{C_3AH_6, \text{ measured}} \approx 422$ (Geiger 2012) J/mol/K

Adequate agreement (estimation!)

measured values preferred > similar solids > VBT

L. Glasser, The effective volumes of waters of crystallization & the thermodynamics of cementitious materials, *Cement*, 3 (2021) 100004.
S. Ghazizadeh, T. Hanein, J.L. Provis, T. Matschei, Estimation of standard molar entropy of cement hydrates and clinker minerals, *Cem Concr Res*, 136 (2020) 106188.
L. Glasser, H.D.B. Jenkins, Predictive thermodynamics for ionic solids and liquids, *Physical Chemistry Chemical Physics*, 18 (2016) 21226-21240 L.

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We can estimate Cp

2) Volume based thermodynamics (VBT); $V_{C_3AH_6} = 149 \text{ cm}^3/\text{mol}$	J/mol/K
Cp (J/mol/K) = $1.1 \cdot S$ for AFm, Glasser 2021)	443 ± 8
<i>Cp (J/mol/K) = $1.1 \cdot S$ for crystalline CSH, Glasser 2021)</i>	<i>343 ± 13</i>
Cp (J/mol/K) = $2.2 \cdot V \text{ (cm}^3/\text{mol}) - 0.8 \text{ solids, Glasser 2016)}$	328 ± 80
Cp (J/mol/K) = from similar solids	449 ± 45 450 ± 45

$C_{p,C_3AH_6, \text{ measured}} \approx 446$ (Geiger 2012), or 459 (Ederova 1979) J/mol/K

Adequate agreement (estimation!)

measured values preferred > similar solids > VBT

L. Glasser, The effective volumes of waters of crystallization & the thermodynamics of cementitious materials, *Cement*, 3 (2021) 100004.
L. Glasser, H.D.B. Jenkins, Predictive thermodynamics for ionic solids and liquids, *Physical Chemistry Chemical Physics*, 18 (2016) 21226-21240 L.

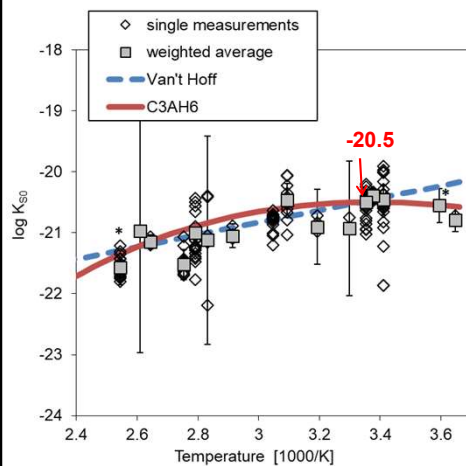
42

Solubility products

1. General considerations
2. Measured concentrations
 $\Leftrightarrow \log K_s$
3. Estimation of C_p and S
4. Calculation of $\log K_s$ at different temperatures

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Solubility of C_3AH_6



$$\log K_T = A_0 + A_2 T^{-1} + A_3 \ln T$$

Van't Hoff equation

2-term extrapolation
(for isoelectric reactions only)

$$\Delta C p_T = \Delta C p_{T_0} = 0$$

$$\log K_T = \frac{0.4343}{R} \left(\Delta_r S_{T_0}^0 - \frac{\Delta_r H_{T_0}^0}{T} \right)$$

$$\text{Log } K_{s0} \text{ } C_3AH_6 = \{Ca^{2+}\}^3 \{Al(OH)_4\}^2 \{OH\}^4$$


Van't Hoff not adequate for non-isoelectric reaction

$$A_0 = \frac{0.4343}{R} \cdot [\Delta_r S_{T_0}^0 - \Delta_r C p_{T_0} (\ln T_0 + 1)]$$

$$A_2 = -\frac{0.4343}{R} \cdot (\Delta_r H_{T_0}^0 - \Delta_r C p_{T_0} T_0)$$

$$A_3 = \frac{0.4343}{R} \cdot \Delta_r C p_{T_0}$$

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Temperature extrapolation

C3AH6						
Ca3Al2O6 (H2O) 6						
	SC	DC				REsDC
0	2	d	a	Al	AlO2-	bn_
1	3	d	a	Ca	Ca+2	an_
2	4	d	a	wX	OH-	bn_
3	4	d	a	w_	H2O@	an_
4	0	n	s	CaAlOH	C3AH6	cem_
5	-1	n	s	CaAlOH	C3AH6	cem_

	V0r			
	-13.264		14.97007	14.97
logK _r	3.162278e-21		-20.5	---
G0 _r	117014.9		-5008155	-5008155
H0 _r	-6634.562		-5537274	---
S0 _r	-414.7222		421.7	421.7
Cp0 _r	-880.3617		445.6	445.6

All information needed can be entered in ReacDC in GEMS

↓

Use RTParm for calculations


$$\log K_T = A_0 + A_2 T^{-1} + A_3 \ln T$$

$$A_0 = \frac{0.4343}{R} \cdot [\Delta_r S_{T_0}^0 - \Delta_r C p_{T_0} (\ln T_0 + 1)]$$

$$A_2 = -\frac{0.4343}{R} \cdot (\Delta_r H_{T_0}^0 - \Delta_r C p_{T_0} T_0)$$

$$A_3 = \frac{0.4343}{R} \cdot \Delta_r C p_{T_0}$$

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 GEM-Selektor ReacDC Setup: s:CaAlOH:C3AH6:cem

Step 1 make a new ReacDC for

ReacDC: Please, set a new record key 1)

s:CaAlOH:C3AH6*:

Phase state code of new Depend

ID of a group to which this new De

Name of this new reaction-defined

Thermodynamic data subset (TDS)

Ok Reset From List

Step 1 - Selection of reaction-defined DC type and codes of methods of T,P correction

Select here the class code for the reaction-defined Dependent Component (DC)

This DC class code will be copied to Phase definition (can be changed there too):

☐ Dependent Component of a single-component condensed phase

The codes set below will configure the ReacDC record and define how to compute T,P corrections for reaction and the new DC it defines.

Select here method codes for T,P correction of standard molar properties of the reaction and DC:

General method code for temperature corrections: **2)**

☒ K Calculation through the logK of reaction TP dependency

Method variant code for temperature EoS corrections:

☒ 3 Three-term extrapolation of logK (T) at dCpr (T) = const

Method code for pressure corrections:

☒ C Molar volume of new DC calculated from constant dVr of reaction

Codes for species-dependent EoS subroutines

☒ N No fluid model routine

Step 2 - Selection of ReacDC/DComp involved in the reaction

To (re)select different species to be involved into reaction, activate the 'Full-list selection' checkbox; toggle it back to see only the selected records again. In the full list, first the ReacDC 'r' and then the DComp 'd' record keys appear; use the filtering settings below to show only relevant records.

☐ Full-list selection

Tick here to see full list

Select all Clear selection

	Source	Aggr.State	Group	Name	Comment
1	d	a	Al	AlO2-	bn_
2	d	a	Ca	Ca+2	an_
3	d	a	wX	OH-	bn_
4	d	a	w_	H2O@	an_

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Step 1: make a new ReacDC for C3AH6

reacDC

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DComp

$\Delta H_{f,C3AH6} \approx -6.6 \text{ kJ/mol}$

$\Delta H_{f,C3AH6} \approx 5537 \text{ kJ/mol}$

DComp :: Thermochemical/EOs data format for Dependent Components

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C3AH6

Ca3Al2O6 (H2O) 6

M0	378.2853	Zz	0
V0d	14.9702		0
G0d	-5008155		2800
H0d	-5537245		2840.346
S0d	421.7		1.6
Cp0d	445.598		0
PrTr	1		25
LamST	---		---
BetAlp	---		---

0 Lothenbach_ea:2012:pap: all log K

1 Taylor:1997:book: V0 (dens)

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C3AH6

Ca3Al2O6 (H2O) 6

	SC	DC			REsDC
0	2	d	a	Al	AlO2-
1	3	d	a	Ca	Ca+2
2	4	d	a	wX	OH-
3	4	d	a	w	H2O
4	0	n	s	CaAlOH	C3AH6
5	-1	n	s	CaAlOH	C3AH6

Adapt r

V0r	-13.264	14.97007	14
logKr	3.162278e-21	-20.5	
G0r	117014.9	-5008155	-5008155
H0r	-6634.562	-5537274	
S0r	-414.7222	421.7	421.7
Cp0r	-880.3617	445.6	445.6
NisoX	---	---	

Log K

Final values as aide memoire

Step 2: Temperature dependence RTParm

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1)

Please, select a source record from:

DComp ReacDC Cancel

ReacDC: Select one key of a source ReacDC record

Please, select one record key. Filter: *

s	CaAlOH	C3AH6	cem
---	--------	-------	-----

2)

s:CaAlOH:C3AH6:cem_r:*

s Phase state of source Dependent Component (DComp or ReacDC)

CaAlOH Group to which source Dependent Component belongs

C3AH6 Name of source Dependent Component

cem_ Code of source thermodynamic data set

r Source of input data for DC { r d }

001 Variant number of this RTParm calculation task <integer>

Ok Reset From List Help Cancel

3) Any number

GEM-Selektor RTparm Setup: s:CaAlOH:C3AH6:cem_:n:001:

Step 1 - Thermodynamic data tabulator (RTParm) configuration

This is a tool for tabulating and plotting thermodynamic data against temperature T and/or pressure P. The input is taken from a DComp or ReacDC record specified in this RTParm record key.

Upon calculation, results will be tabulated on the 'Tables' page, as specified in 'tExpr' math script. Results can be plotted, exported into text files, or copy-pasted to other programs.

Simple 'tExpr' scripts can be created using a selection dialog on the next page of this wizard. Example scripts are also provided under 'Help' 'View Scripts...' menu command in the RTParm window.

2) T then P increments Select mode for iterating xP and xT arguments. Default mode: 2.

Temperature T

Units: C Celsius

Minimal: 0.00

Maximal: 100.00

Step: 5.00

Number of points: 21

☒ Plot as abscissa xT

Pressure P

Units: b bar

Minimal: 1.00

Maximal: 1.00

Step: 0.00

Number of points: 1

☐ Plot as abscissa xP

Learn more < Back Next> Cancel

Step 2 - Selection of items to sample (to retain the old script, just click 'Next >')

Property: Scalars

Item Selection:

twG	twEw
twH	twRT
twS	twP
twCp	twTC
twV	twTK
twK	tw[0]
tlogK	xT
tdGr	xP
tdHr	
tdSr	
tdCpr	
tdVr	
twRow	

List of static data objects (see tooltip on each object name)

Sampling Script: yF[jTP][0] =: tlogK;

Select tlogK

Learn more < 1

14 datapoints

Step 3 - Important dimensions

Setup of dimensions for data tabulation arrays

1 Number of columns in the yF table (plot curves), 1 Number of rows (T,P pairs) in yF, xP, xT arrays will be

14 Optional: Number of rows in xTE, xPE, yTE arrays for Default: 0 (arrays not provided).

1 Optional: Number of columns in yTE array for expe

Temp	Matschei: under
5	-20.39
25	-20.45
55	-20.78
70	-21.24
85	-21.60
105	-22.18

Temp	Matschei: over
5	-20.65
25	-20.40
40	-20.64
50	-20.47
70	-21.20
85	-21.49
90	-21.47
110	-22.15

Scripts Tables TPwork **Setup**
23/05/2023, 17:16

T (and P) corrections: log K function of C3AH6

Please, change the script and/or remake, if necessary

rpUn r j j b C + T C b -

rpNpT 1 21 21

rpMode

rpSize 0 0

rDimXY 21 1

rDimEf 14 1

tYName kJ/m

tExprE
Experimental data can be entered

tXName C Celsius Plot 1

	xTE	xPE	ytE
0	5	1	-20.39
1	25	1	-20.45
2	55	1	-20.78
3	70	1	-21.24
4	85	1	-21.6
5	105	1	-22.18
6	5	1	-20.65
7	25	1	-20.4
8	40	1	-20.64

As calculated in
Lothenbach ea 2012 CCR 42

T (and P) corrections: log K function of C3AH6

Calculated value

$C_{p,C3AH6, \text{measured}} \approx 446$ (Geiger 2012)

$S_{C3AH6, \text{measured}} \approx 422$ (Geiger 2012),

Good agreement!

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Empa
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Step 3: make an additional ReacDC for C3AH6

«C3AH6.cem2»

$C_{p,C3AH6} \approx 328$ (Glasser 2016)
 $S_{C3AH6} \approx 399$ (Glasser 2016)

$\Delta H_{f,C3AH6} \approx 0.3 \text{ kJ/mol}$ ←

Adapt Sr, Cpr

Clone the entry in RTParm
 And link it to the new ReacDC

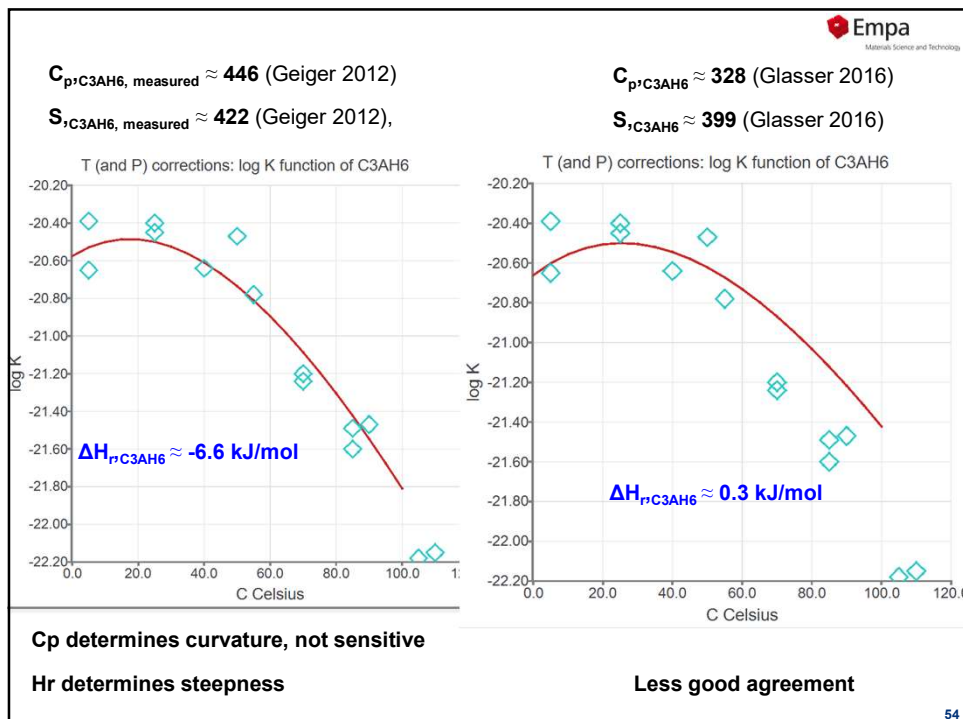
Page 1 Page 2 23/05/2023, 17:27

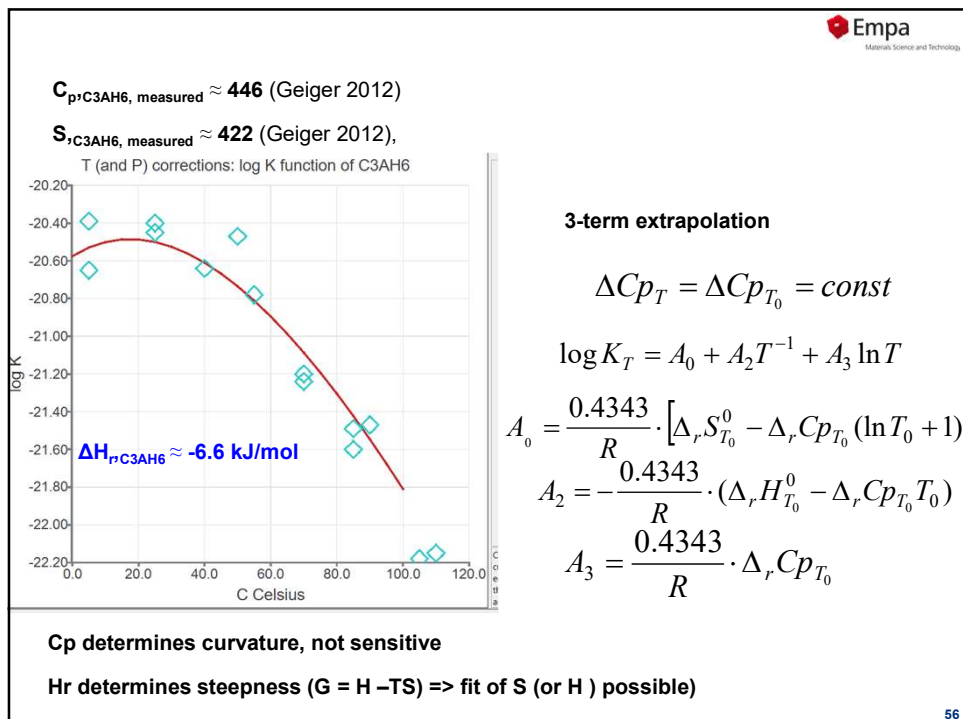
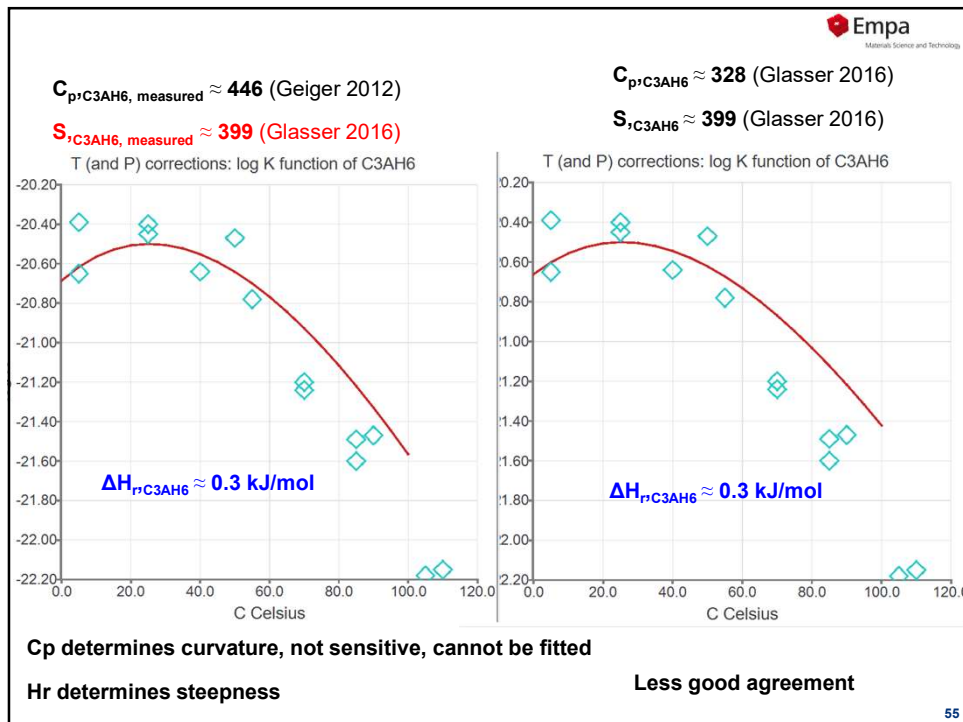
C3AH6
 $\text{Ca}_3\text{Al}_2\text{O}_6(\text{H}_2\text{O})_6$

	SC	DC				REsDC
0	2	d	a	Al	AlO2-	bn_
1	3	d	a	Ca	Ca+2	an_
2	4	d	a	wX	OH-	bn_
3	4	d	a	w_	H2O@	an_
4	0	n	s	CaAlOH	C3AH6	cem2
5	-1	n	s	CaAlOH	C3AH6	cem2

Final values as aide memoire

V0r	-13.264	14.97007	14.97
logKrr	3.162278e-21	Log K	-20.5
G0r	117014.9	-5008155	-5008155
H0r	282.5218	-5544192	---
S0r	-391.5222	398.5	398.5
Cp0r	-762.5617	327.8	327.8
NiscX	---	---	---





Measured enthalpy values for C3AH6

Measured ΔH

- -5562 \pm 5 kJ/mol, Berman 1961
- -5548 kJ/mol, Abramov 1981
- -5552 \pm 16 kJ/mol, Schoenitz 1999

		Calculated ΔG	log K
↓			
• -5552 kJ/mol, Geiger 2012	=>	-5021 kJ/mol	=> -22
Calculated ΔH		Calculated ΔG	log K
• -5537 kJ/mol, Lothenbach 2012	<=	-5008 kJ/mol	<= -20.5
Corrected G° for Al^{3+}		Calculated ΔG	log K
• -5546 kJ/mol, in progress	<=	-5017 kJ/mol	<= -20.5

Measured enthalpy values associated with considerable error

± 16 kJ/mol (of ΔG) => correspond to 3 log units in K_{so} !

log K preferable (as G depends on other data)

Berman, H. A., Newman, E. S., Heat of formation of calcium aluminate monocarbonate at 25 °C, J Res Nat Bur St-A. Phys Chem 65A, (1961), 197-207
 Abramov, V. Y., Alekseev, A. I., Values of thermodynamic properties of calcium hydrogarnets of the composition $3CaO \cdot Al_2O_3 \cdot xSiO_2 \cdot (6-2x)H_2O$, J Appl Chem USSR 54, (1981), 812-815
 Schoenitz, M., Navrotsky, A., Enthalpy of formation of katoite $Ca_3Al_2[(OH)_4]_3$: Energetics of the hydrogarnet substitution, Am Min 84, (1999), 389-391
 Geiger, A. C., Dachs, E., Benisek, A., Thermodynamic behavior and properties of katoite (hydroglossular): a calorimetric study, Am Min 97, (2012), 1252-1255.
 Lothenbach, B., Pelletier-Chagnat, L., Winnefeld, F., Stability in the system $CaO-Al_2O_3-H_2O$ CCR 42, (2012), 1621-1634.

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Conclusions solubility products

Do under- and oversaturation experiments

Measure at different temperatures

⇒ Use GEMS to calculate log K and ΔG

Compare to existing literature !

(if possible recalculate based on measured concentrations)

⇒ If available, use measured S and C_p for temperature extrapolation

⇒ Else estimate from similar solids (if possible)

⇒ if not, use VBT

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